

# Peculiarities of TiH<sub>2</sub> decomposition

Emília Illeková · Jana Harnúšková ·  
Roman Florek · František Simančík ·  
Igor Maňko · Peter Švec Sr.

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**Abstract** The eventual competition between the dehydrogenation and oxidation of TiH<sub>2</sub> powder in the argon, oxygen, and static air atmospheres has been examined in the regime of linear heating using differential thermal analysis (DTA), X-ray diffraction, transmission and scanning electron microscopy coupled to energy dispersive spectroscopy techniques. Three stages of dehydrogenation, R1, R2, and R3, and two different oxidation reactions, O1 and O2, have been identified. The kinetics of individual reactions has been investigated by the Kissinger and Suriñach curve fitting procedures. While the kinetics of O1, O2, and R1 reactions depends on the diffusivities of the external reagent gas, being oxygen, and internal product gas, being hydrogen, the main dehydrogenation stage R2 is controlled by the combined nucleation-and-growth and coalescence kinetics. The effect of pre-annealing of TiH<sub>2</sub> on its subsequent degradation has also been studied. Due to the huge overheating accompanying both oxidation reactions in the DTA set-up, substantial thermal losses have been demonstrated and the method to obtain the true heat of oxidation reactions in metals has been described.

**Keywords** Titanium hydride · Dehydrogenation · Oxidation · DSC · Kinetics

## Introduction

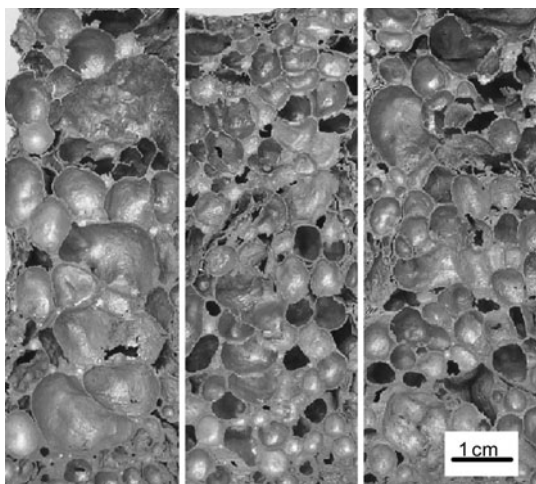
At elevated temperatures titanium hydride (TiH<sub>2</sub>) gradually decomposes via a two-stage endothermic reaction evolving H<sub>2</sub> and yielding pure titanium. As the decomposition proceeds between 673 and 1073 K, i.e., at temperatures close to the melting temperatures of aluminum-based alloys, its products find metallurgical exploitation [1]. Namely, due to the progressive evolution of H<sub>2</sub> bubbles in time of the melting and solidification of aluminum (or aluminum-based alloys), the foamy form of Al can be produced. It is sure that the decomposition kinetics directly affects the foaming kinetics, see Fig. 1 [2]. Moreover, in the open air atmosphere, certain relation between the dehydrogenation and the oxidation of titanium should exist [1, 3].

Generally, the decomposition of a metal hydride under non-equilibrium conditions (at linear heating) is a multi-stage process, the mechanism of which is scarcely studied. Generally, differential scanning calorimetry (DSC) is being used for such studies [1, 3–6]. The thermal desorption spectroscopy (TDS) analyses of Fernandez et al. showed linear proportionality between the hydrogen evolved (TDS data) and the heat absorbed (DSC data) in the case of dehydrogenation of TiH<sub>2</sub> [4]. Later, also the reaction model for TiH<sub>2</sub> dehydrogenation was deduced and the rate-controlling process supposed by estimating the activation energy and its variation using the isoconversional method and the thermogravimetry data (TG) by Liu et al. [3].

In this article, the details in the kinetics of the dehydrogenation as well as of the high-temperature oxidation of powdered TiH<sub>2</sub> are studied by the use of the DSC technique. Experimental data are analyzed by the Suriñach curve fitting procedure [7]. The specific roles as well as the mutual relation between the dehydrogenation and the oxidation reactions are investigated.

E. Illeková (✉) · I. Maňko · P. Švec Sr.  
Institute of Physics, Slovak Academy of Sciences,  
Dúbravská cesta 9, 845 11 Bratislava, Slovakia  
e-mail: fyziille@savba.sk  
URL: <http://www.savba.sk/rq>

J. Harnúšková · R. Florek · F. Simančík  
Institute of Materials and Machine Mechanics, Slovak Academy  
of Sciences, Bratislava, Slovakia



**Fig. 1** Al foam with **a** TiH<sub>2</sub> without heat-treatment, **b** TiH<sub>2</sub> heat-treated in air for 15 min at 673 °C, **c** at 718 °C

## Materials and methods

Commercial titanium hydride powder, TiH<sub>2</sub>, supplied by Chemetall GmbH, Frankfurt (purity 98.8%, nominally <63 μm, average particle size  $d = 5 \mu\text{m}$ ) was examined in the as-produced state and also after various industrial pre-treatments. Pre-treatments were done in industrial-size batches isothermally at 673, 718, or 788 K for 15 min in static air atmosphere. Alternatively, TiH<sub>2</sub> powder produced by Alulight ( $d \sim 63 \mu\text{m}$ , fraction) was measured.

The thermodynamic stability and the kinetics of observed phase transformations were monitored by high-temperature differential thermal analyzer (DTA) in the mode of DSC using Perkin-Elmer DTA7. Linear-heating regimes using six heating rates,  $\Phi$ , from 1 to 30 K min<sup>-1</sup> at temperatures,  $T$ , between 300 and 1123 K were used. After the calibration, the error of established quantities is  $\pm 2 \text{ K}$  and  $\pm 4 \text{ J g}^{-1}$  for all heating rates. Three types of experiments were realized: (i) the dehydrogenation was followed by measurements in dynamic argon (30 mL min<sup>-1</sup>), (ii) the oxidation was attained by measuring in dynamic oxygen (30 mL min<sup>-1</sup>), (iii) the degradation of TiH<sub>2</sub> under non-equilibrium conditions, similar to the industrial ones, was carried out by measuring in static air. Both the input of the reacting gas O<sub>2</sub> and the output of the released gas H<sub>2</sub> were accomplished by locating of always the same big mass of the powdered sample (26 mg) in narrow (3 mm) and deep (7 mm) alumina pans without lids.

The structure of initial, partially heat-treated and product powders was evaluated by X-ray diffraction (XRD) using Cu K<sub>z</sub> radiation at room temperature. The structural and chemical analysis of both initial TiH<sub>2</sub> and pre-treated powders were performed by scanning electron microscopy coupled to energy dispersive spectroscopy technique

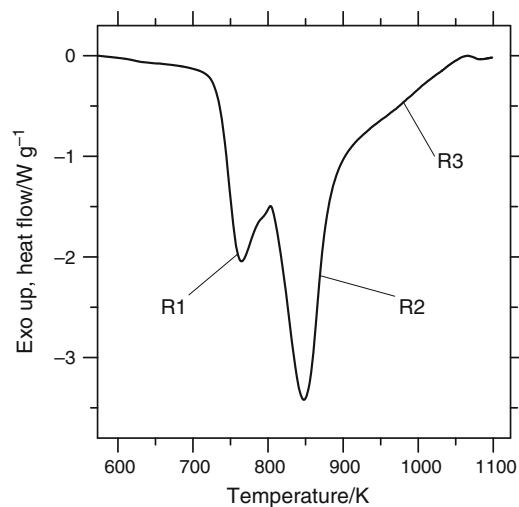
(SEM/EDX) using SDB Quanta 3D 200i. More detailed analysis of pre-treated powders was performed by transmission electron microscopy (TEM) using JEOL 2000 FX.

## Results and discussion

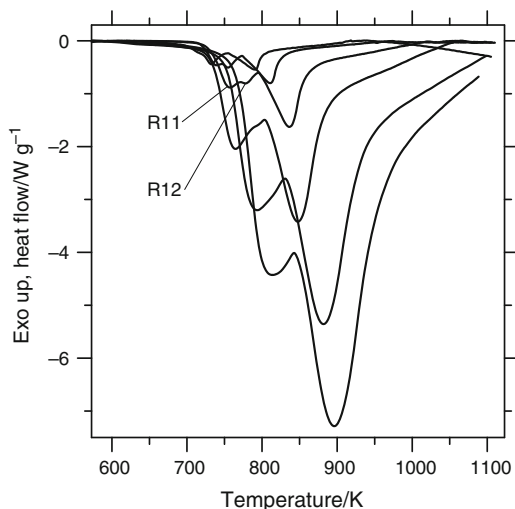
### Dehydrogenation

Figure 2 shows a typical DSC curve of TiH<sub>2</sub> measured in argon. The dehydrogenation is represented by a massive complex endothermic double peak ( $\Delta H \sim 2600 \text{ J g}^{-1}$ ) which starts at the temperature  $T_x > 700 \text{ K}$  and is finished above 1123 K, the highest temperature of our measurements. Accordingly with Borchers et al. or Liu et al. [3, 8], three transformation stages, R1, R2, and R3, have been identified. This principal character of the decomposition is independent of the heating rate, as is seen in Fig. 3. Moreover, looking at the details, we were able to distinguish two sub-peaks, R11 and R12, in each DSC curve. The temperatures of the maxima,  $T_{p11}$ , and  $T_{p12}$ , of these two minor thermal effects being shallow and weak, clearly follow straight lines in the Kissinger heating rate dependence [9] (Fig. 4). We used Kissinger and Elder methods [9, 10] to calculate the activation energies,  $E^*$ , and pre-exponential factors,  $A$ , for R11, R12, and R2 transformation stages. They are summarized in Table 1.

DSC curves in Fig. 5 show that, after the pre-heating at appropriate temperature,  $T_a$ , the multistage dehydrogenation is gradually reacted out, the complex endothermic effect starts at  $T_x > T_a$  consuming less heat (and giving less



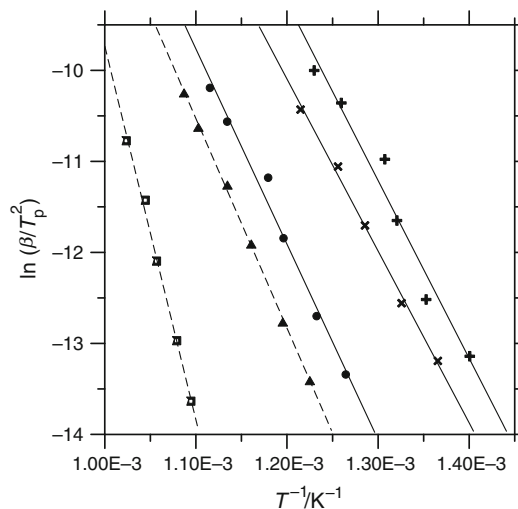
**Fig. 2** Subtracted (first minus second run) DSC linear-heating curve from as-produced TiH<sub>2</sub> powder taken at 10 K min<sup>-1</sup> in argon. Dehydrogenation stages (endothermic peaks) R1, R2, and R3 are identified



**Fig. 3** Heating rate dependence of the DSC curve for as-produced TiH<sub>2</sub> powder. Measurements were done in argon. Heating rates are 1, 2, 5, 10, 20, and 30 K min<sup>-1</sup>

hydrogen as well [4]). The more extensive is the sample thermal pre-treatment, the less is the remaining total reaction gain in the following measurement. Moreover, in contrast to any pre-treatment in argon [1, 8], the annealing in air, anticipating the presence of oxidation, slightly shifts the following complex endothermic effect to higher temperatures. That shift suggests certain retardation in the dehydrogenation kinetics. The shape of DSC curves (measured in argon) of pre-treated samples does not depend on the heating rate. The Kissinger heating rate dependence of the peak temperature of the R2<sub>(788,15)</sub> transformation stage (being the R2 stage of the sample isothermally pre-treated in air at 788 K for 15 min) is in Fig. 4, too, and the deduced  $E_{2,(788,15)}^*$  and  $A_{2,(788,15)}$  are in Table 1.

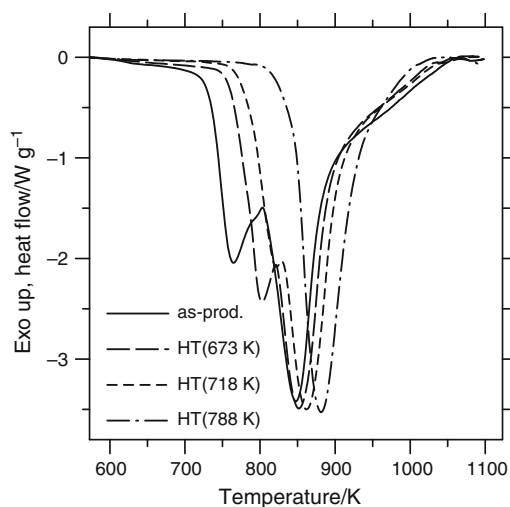
All calculated activation energies being 157–192 kJ mol<sup>-1</sup> can be compared with values reported earlier [3, 8, 11]. The obtained evolution of the activation energy with temperature coincides with the values found in [8] or [11] but it contradicts to the dependence deduced by isoconversional methods in [3]. However, as mentioned above, our results gave evidence that the R1 stage consists of two individual sub-stages the extents of which depend on the heating rate (see Fig. 3), and the independence of R1, R2, and eventual higher temperature stages has not been disproved yet. Therefore, we suppose that the variation of an apparent activation energy with temperature, i.e., with the total extent of conversion,  $\alpha$ , estimated by any isoconversional method might be only virtual in this specific case. Moreover, our results and all other previous results yielded increased  $E^*$  (~7% in this article) in the case of the presence of oxides in the TiH<sub>2</sub> sample. Thus, the relevant variability in absolute values of  $E^*$ , presented in the referred article, might be interpreted also by this reason.



**Fig. 4** Linear Kissinger-Elder plots for determination of activation energies and frequency factors of dehydrogenation stages R11 (plus), R22 (times), R2 (filled circle) in as-produced and R2<sub>(788,15)</sub> (filled triangle) in pre-treated at 788 K for 15 min in air TiH<sub>2</sub> powder. Also the apparently linear dependence for oxidation reaction O2 (open square) is shown. DTA measurements were done in argon

**Table 1** Activation energies and pre-exponential factors for dehydrogenation of as-produced (R11, R12, R2), pre-treated at 788 K for 15 min (R2<sub>(788,15)</sub>) and for oxidation (O2) of TiH<sub>2</sub> powder

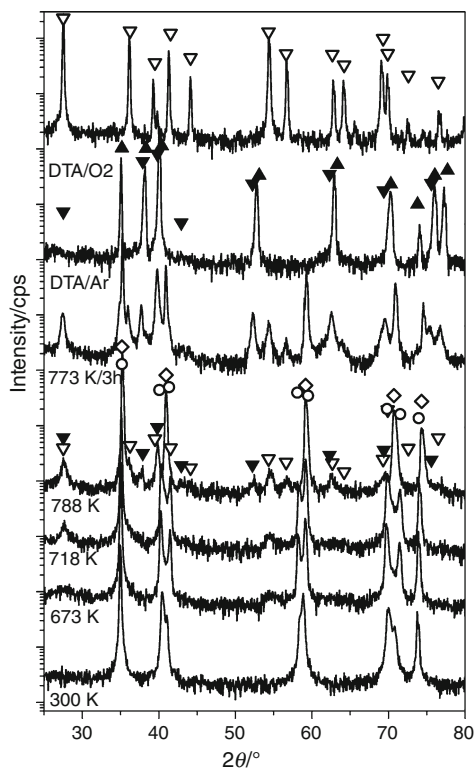
Reaction stage	$E^*/\text{kJ mol}^{-1}$	$A/\text{s}^{-1}$
R11	162 ± 15	5.0 × 10 <sup>8</sup>
R12	157 ± 6	9.5 × 10 <sup>7</sup>
R2	179 ± 11	3.9 × 10 <sup>8</sup>
R2 <sub>(788,15)</sub>	192 ± 3	1.1 × 10 <sup>9</sup>
O2	341 ± 13	2.9 × 10 <sup>16</sup>



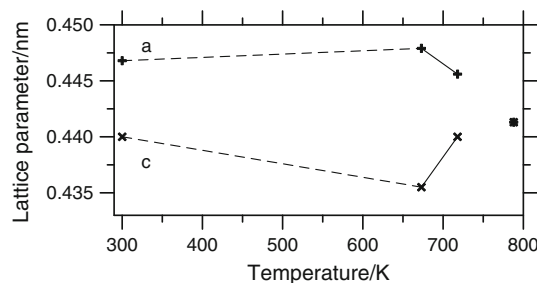
**Fig. 5** DSC linear-heating curves of TiH<sub>2</sub> powder pre-treated in air for 15 min taken at 10 K min<sup>-1</sup> in argon. Annealing temperature is the parameter. Curve for untreated powder is also shown

XRD spectra of our as-produced and pre-treated samples (see Fig. 6) evidenced the presence of oxides, namely  $\text{Ti}_6\text{O}$  and  $\text{TiO}_2$  (rutile), in the  $\text{TiH}_2$  powder. Weak oxygen traces are already in the non-treated samples. The original Ti-hydride containing 1.924H/Ti has been identified as tetragonal  $\varepsilon$ -phase. Increasing the temperature, the  $\text{TiH}_2$  starts to decompose,  $\text{H}_2$  continuously leaves the rigid titanium lattice and both lattice parameters,  $a$  and  $c$ , continuously change (Fig. 7). Finally, for example, after annealing at 788 K for 15 min, the cubic  $\delta$ - $\text{TiH}_{1.5}$  is detected ( $a = 0.4413$  nm). Simultaneously in the presence of an oxygen containing atmosphere, oxygen probably transforms the original lattice with abundance of vacant sites due to released hydrogen and thus increases the content of Ti oxides. At elevated temperatures, due to the advanced escape of  $\text{H}_2$ , the  $\beta$ -Ti(H) should be formed [3, 8]. At the end of our DTA experiments, the dehydrogenation has been finished and the stable  $\alpha$ -Ti is obtained.

SEM images in Fig. 8a and b show that the pre-treatment in air significantly influenced neither the  $\text{TiH}_2$  particle size nor the morphology of the particle surface. However, EDX analysis evidenced the presence of oxygen in pre-treated powder. The TEM analysis detected the



**Fig. 6** XRD diffraction patterns of as-produced and heat-treated  $\text{TiH}_2$  powder. Heat-treatment is the parameter. Open circle  $\varepsilon$ - $\text{TiH}_{1.924}$ , open diamond  $\delta$ - $\text{TiH}_{1.5}$ , filled triangle  $\alpha$ -Ti, filled inverted triangle  $\text{Ti}_6\text{O}$ , open triangle  $\text{TiO}_2$



**Fig. 7** Dependence of lattice parameters of tetragonal  $\varepsilon$ - $\text{TiH}_{1.924 \rightarrow 1.5}$  powder on temperature of isothermal annealing. Annealing time was 15 min. Dashed lines reflect the effect of lattice dilatation, solid lines represent the dehydrogenation of  $\varepsilon$ -phase, the points at 788 K correspond already to the  $\delta$ -phase

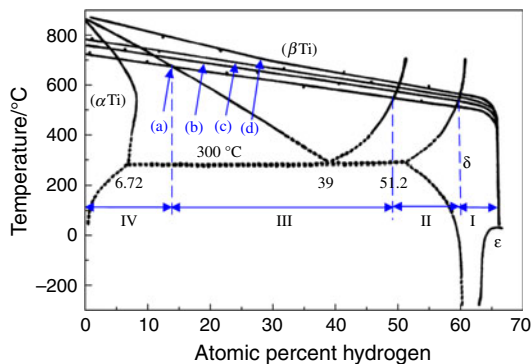
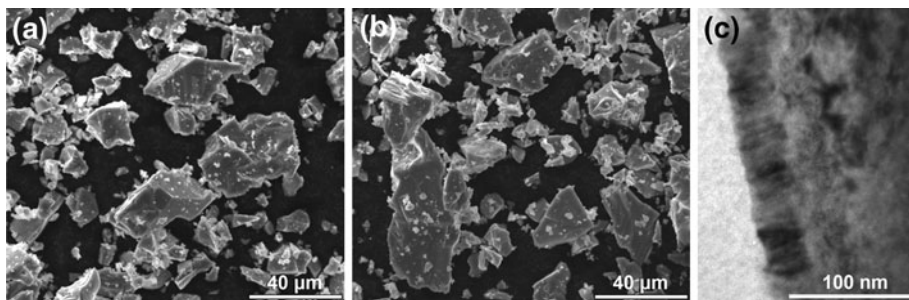
oxygen being just in the columnar oxide layer systematically growing into each particle from its surface, Fig. 8c.

On the base of our results, we can apply and develop the reaction model for the non-isothermal dehydrogenation of  $\text{TiH}_2$  powders introduced in Liu et al. [3] and supported by Fig. 9. Because the reactivity between the oxygen and titanium is high, the Ti lattice tends to “absorb” eventual  $\text{O}_2$  molecules from the surroundings throughout each particle surface. Simultaneously at  $T > T_x$ , the powders decompose releasing  $\text{H}_2$ . First, in the R11 sub-stage, the  $\varepsilon$ - $\text{TiH}_x$  phase changes its composition  $\text{TiH}_{1.924 \rightarrow 1.5}$  being then transformed into  $\delta$ - $\text{TiH}_{1.5}$  phase in the R12 sub-stage. In the R2 stage, the  $\beta$ -Ti(H) is formed which is finally transformed into  $\alpha$ -Ti(H) and  $\alpha$ -Ti in the R3 stage. Dehydrogenation and oxidation are not competitive but rather consecutive reactions in the case of Ti hydride. It means that oxygen (if present) transforms gradually the tetragonal  $\text{TiH}_2$  lattice into the tetragonal  $\text{TiO}_2$  (rutile) via formation of pure Ti and  $\text{Ti}_6\text{O}$ ; however, simultaneously, the new formed Ti–O surface layer slows down the further escape of  $\text{H}_2$ . While the R11 transformation might proceed continuously from each particle surface into its center as has been suggested in Liu et al. [3], there is not such reason in the case of the formation of  $\beta$ -Ti(H) or  $\alpha$ -Ti(H) grains. Thus, in any moment, the variable local composition, (variable local lattice parameter, physical properties, etc.) as well as variable local extend of conversion should exist.

In any case, the relation between the local mechanisms being diffusion [1], surrounding/particle interface reaction [3] or any nucleation and growth mechanisms and the overall rate-controlling mechanism need not to be elementary. It should be searched and, for example, by the DSC kinetic analysis deduced. We have used the Suriñach curve fitting procedure [7]. In this way, each single DSC curve (continuous heating or isothermal) represented in an appropriate coordinate system should correlate with the same master-curve, which is fitted by the most probable theoretical one. The Suriñach analysis of the simplest DSC



**Fig. 8** SEM images of TiH<sub>2</sub> powder ( $d < 63 \mu\text{m}$ ): **a** as-produced; **b** pre-treated in air at 788 K for 15 min. **c** TEM image of the TiH<sub>2</sub> powder particle ( $d < 63 \mu\text{m}$ ) pre-treated in air at 788 K for 15 min. The electron diffraction patterns (not shown) identified TiO<sub>2</sub> in the surface layer and  $\delta$ -TiH<sub>1.5</sub> in the core

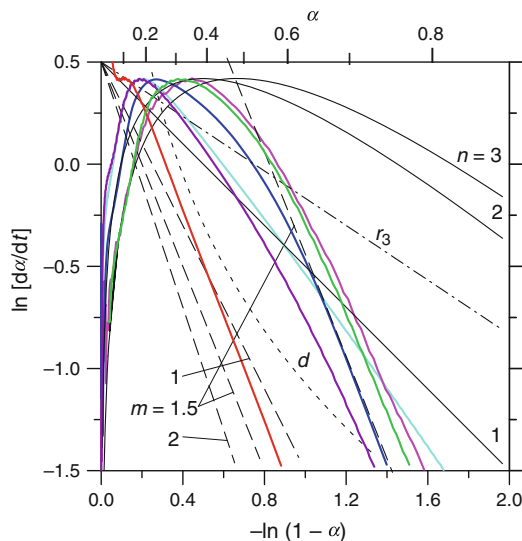


**Fig. 9** Ti-H phase diagram combined with the TG curves: **a** 10 K min<sup>-1</sup>, **b** 15 K min<sup>-1</sup>, **c** 20 K min<sup>-1</sup>, **d** 40 K min<sup>-1</sup> [3]

curve (the dash-and-dotted line in Fig. 5), being the R2<sub>(788,15)</sub> dehydrogenation stage, is in Fig. 10. It is seen that the Suriñach plots for the six heating rates do not follow one master-curve even in this case. However, they certainly do not represent any diffusion-controlled kinetics (being a convex curve) and they neither represent any interface reaction controlled kinetics (being a straight line). In contrast, they might follow the Johnson–Mehl–Avrami nucleation and growth kinetics [12] with a heating rate dependent exponent  $n(\Phi)$ .  $n$  being initially 3 (three-dimensional interface-controlled growth of already nucleated  $\beta$ -Ti particles or, more probably, decaying homogeneous nucleation and diffusion-controlled three-dimensional growth of the  $\beta$ -Ti phase) should dramatically decrease with proceeding extent of conversion,  $\alpha$ . Finally, the JMA kinetics should revert into the normal grain-growth one reaching the exponent  $m = 1.5$  (coalescence controlled by the solution of the second phase matrix [13], i.e., coalescence of  $\beta$ -Ti grains in the continuously degrading  $\delta$ -TiH<sub>1.5</sub> surroundings). Such result might be accepted taking into account the compositional inhomogeneity in each particle as well as the presence of the R3 stage at higher temperatures.

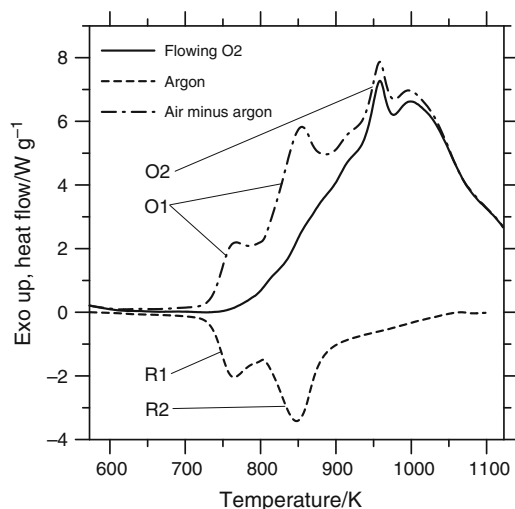
#### Oxidation

The typical DSC curve from the linear-heating measurement of TiH<sub>2</sub> powder in oxygen is the full-line in Fig. 11. The XRD spectrum (Fig. 6) of the powder after such DTA



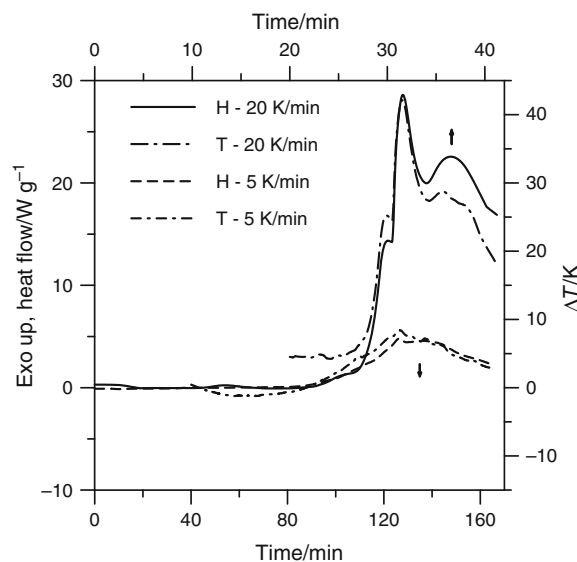
**Fig. 10** Suriñach representation of linear-heating dehydrogenation effect R2<sub>(788,15)</sub> in TiH<sub>2</sub> powder pre-heated in air at 788 K for 15 min. Colored curves DTA measurements in argon at 1 K min<sup>-1</sup> (solid pink line), 2 K min<sup>-1</sup> (solid green line), 5 K min<sup>-1</sup> (solid blue line), 10 K min<sup>-1</sup> (solid red line), 20 K min<sup>-1</sup> (solid violet line), and 30 K min<sup>-1</sup> (solid turquoise line). Black lines are the theoretical curves for various rate-controlling kinetic laws: JMA nucleation-and-growth (solid line) where  $n$  is the parameter, interface reaction  $r_3$  (dash-and-dotted line), diffusion  $d$  (small dashed line) and normal-grain-growth (big dashed line) where  $m$  is the parameter. The lines are vertically shifted to match with the experimental curves. (Color figure online)

measurement shows only the TiO<sub>2</sub> lines. This has attested that both oxidation and dehydrogenation had to take place. Accepting the additivity of thermodynamic quantities and knowing the kinetics of the dehydrogenation (dash-line in Fig. 11), the DSC curves obtained in oxygen and argon atmospheres could be subtracted and the kinetic evolution of the oxidation extracted; it is the dash-and-dotted line in Fig. 11. Thus, the oxidation forms the complicated and large exothermic peak ( $\Delta H \sim -13999 \text{ J g}^{-1}$  at  $\Phi = 10 \text{ K min}^{-1}$ ). It has been divided into two oxidation effects, O1 and O2. The major reaction, O1, is slow; it follows the dehydrogenation kinetics, where both R1 and R2 stages are visible. Probably, it reflects the continuous consecutive replacement of escaping hydrogen by oxygen through a sequence of Ti oxides, finally forming rutile. The reaction O2 is sharp having the explosive character. Both reactions

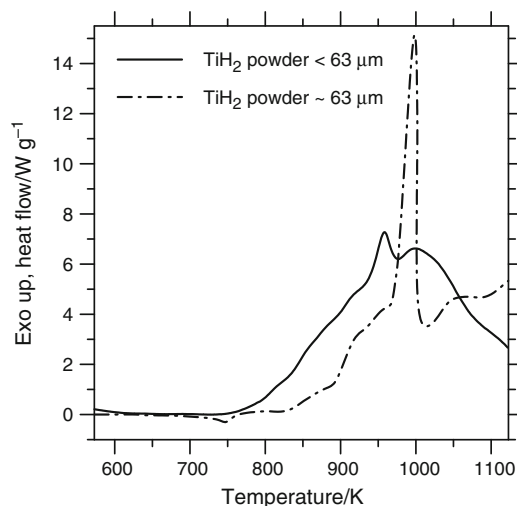


**Fig. 11** Subtracted (1 run minus 2 run) DSC linear-heating curve from as-produced  $\text{TiH}_2$  powder taken at  $10 \text{ K min}^{-1}$  in flowing oxygen (solid line). Also the measurement in argon (small dashed line) and the subtraction of data taken in  $\text{O}_2$  and Ar (dash-and-dotted line) are shown. Oxidation reactions (exothermic peaks), O1 and O2, are identified

O1 and O2 have been observed at each heating rate. However, the individual heats,  $\Delta H_{\text{O1}}$ ,  $\Delta H_{\text{O2}}$ , are not constant (see Table 2). In any case, the evolved oxidation heat is huge and in the course of DTA experiment it gives rise to considerable overheating of the sample,  $\Delta T$ , with relation to its surroundings. The absolute value of  $\Delta T(T)$  dependence is shown in Fig. 12. Moreover, due to the reaction kinetics  $\Delta T$  realized in the DTA instrument increases with increasing  $\Phi$ . Thus, for example,  $\Delta T = 40 \text{ K}$  in the case of  $\Phi = 20 \text{ K min}^{-1}$  (and  $\sim 380 \text{ K}$  if  $\Phi = 30 \text{ K min}^{-1}$ ). However, the higher temperature gradient between the sample and the surrounding invokes the higher thermal losses across the interface. This variability in the non-trivial thermal losses toward the sample's surrounding might be responsible for the variability in the measured reaction heats as, for example, in the case of  $\Delta H_{\text{O1}}$  (see Table 2). Therefore, the DTA should record apparent oxidation effects, which consist of the true, constant reaction heat and the variable thermal losses (in fact a difference between the



**Fig. 12** Proportion between the heat effects, calculated by the DSC mode from the DTA data (H, full-and-dashed lines) and over-heatings (T, dash-and-dotted lines) of O1 and O2 reactions in as-produced  $\text{TiH}_2$  powder taken in DTA in flowing oxygen. Heating rate is the parameter. Arrows indicate the corresponding time axes



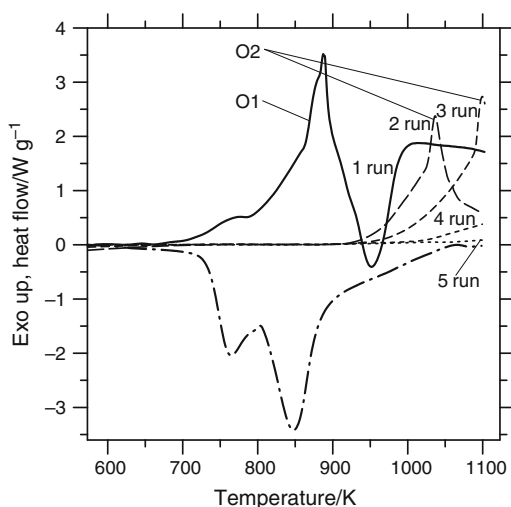
**Fig. 13** Variability of the oxidation kinetics with the quality of the as-produced  $\text{TiH}_2$  powder. Diameter of the grains is the parameter. Taken in DTA at  $10 \text{ K min}^{-1}$  in flowing oxygen

**Table 2** Heats of O1 and O2 oxidation reactions, and the overheating produced in  $\text{TiH}_2$  powder as dependences of heating rate

$\Phi/\text{K min}^{-1}$	$\Delta H_{\text{O1}}/\text{J g}^{-1}$	$\Delta H_{\text{O2}}/\text{J g}^{-1}$	$\Delta T_{\text{O2}}/\text{K}$
1	-9017	-997	0.9
2	-10551	-391	1.0
5	-13038	-67	0.7
10	-13707	-294	3.7
20	-14282	-1334	14.5
30			381.1

thermal losses of the sample and the reference) increasing proportionally to  $\Delta T$ . Then, the true  $\Delta H_{\text{O1}}$  might be obtained extrapolating its dependence on  $\Delta T$  to zero.

The reaction O2 seems to be more complicated. The proportionality between  $\Delta H_{\text{O2}}$  and  $\Phi$  is not simple (see Table 2). Moreover, the onset temperature,  $T_{\text{x,O2}}$ , and heat effect of O2 depend on the quality of the  $\text{TiH}_2$  powder as it can be seen in Fig. 13 and on the purity of the atmosphere too. In any case, increasing  $T_{\text{x,O2}}$  increases also the  $\Delta H_{\text{O2}}$  at the expense of  $\Delta H_{\text{O1}}$ . Due to this fact, the kinetic



**Fig. 14** Sequence of 6 subtracted (current minus 6th run) DSC linear-heating curves from as-produced TiH<sub>2</sub> powder taken at 10 K min<sup>-1</sup> in static air. Oxidation reactions (exothermic peaks) O1 and O2 are identified. Also the measurement in argon (dash-and-dotted line) is shown

parameters of O2 determined by Kissinger–Elder methods (Fig. 4) and presented in Table 1 might be false. We suppose that the appearance of this explosive reaction might be related to the dimensions of the powder grains, i.e., to their diameter, surface, or volume. The O2 reaction is independent of the pre-treatment and it proceeds in dehydrogenated samples too (in this case above 1042 K). It means that it is either independent of the presence of hydrogen, it appears when  $\alpha$ -Ti starts to be formed, or it is initialized when the escape of H<sub>2</sub> is finished.

#### TiH<sub>2</sub> degradation in static air

As shown above, the decomposition of TiH<sub>2</sub> powder proceeds independently of the atmosphere. Contrariwise, the oxidation is dependent on the access of oxygen. The more hindered is the oxygen inlet, the slower and more peculiarly the oxidation manifests itself. Thus, for example, in the case of linear heating in static air when the sample lies deeply in a profound container (sample pan), the oxidation starts regularly and then stops above 900 K when all oxygen, located in the container, has been reacted and the stream of liberated hydrogen prevents further inlet of additional oxygen (the full-line up to 950 K in Fig. 14). Later, when the dehydrogenation is completed (represented by the endothermic dash-and-dotted line in Fig. 14), a new O<sub>2</sub> molecule might reach the sample and the oxidation might continue at higher temperatures again (the full-line above 950 K in Fig. 14). But in any case, the O2 reaction does not start and the rate of the O1 reaction is limited by

the partial diffusivity of O<sub>2</sub> molecules in the ambient air. Therefore, the typical plateau in the DSC curve is formed [14]. The O2 reaction can start in the next heating run and both reactions only slowly decay in the sequence of several subsequent heating runs.

#### Conclusions

In the oxygen containing atmosphere, two consecutive reactions, namely the dehydrogenation and the oxidation, take part in TiH<sub>2</sub> powder at approximately same elevated temperatures.

- Dehydrogenation is initialized by temperature. It advances continuously, from the surface of each particle to its center, having three distinct stages (R1, R2, and R3). The major decomposition stage, R2, is controlled by the JMA nucleation-and-growth and modified coalescence reaction kinetics. The dehydrogenation might be slightly decelerated by eventual oxidation.
- Appropriate thermal treatment shifts the dehydrogenation to higher temperatures; however, it lowers the gain of hydrogen.
- Oxidation takes place consecutively, having two types (O1 and O2). O1 reaction is slow; it is controlled by the kinetics of the dehydrogenation. O2 reaction is explosive; its initialization temperature depends on the morphology of the TiH<sub>2</sub> powder. The overall oxidation produces giant heat causing risky overheating.
- Oxidation slightly shifts the dehydrogenation to higher temperatures. Limiting the supply of oxygen does not influence the dehydrogenation; however, it might control the oxidation and its heat production.

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#### Appendix

(i) The Kissinger–Elder relation [9, 10] is

$$\ln \left[ \Phi / T_p^2 \right] = \ln[(AR)/E^*] + \ln f_m(\max) - E^*/(RT_p),$$

where  $A$  and  $E^*$  are parameters being pre-exponential factor and activation energy,  $\Phi$  is the heating rate,  $T_p$  is the DSC peak temperature,  $R$  is the gas constant and  $\ln f_m(\max) = -0.485$ .

(ii) The Suriñach representation [7] is

$$\ln[d\alpha(T, t)/dT] + [E^*/RT(t)] + \ln \Phi \text{ versus} \\ - \ln [1 - \alpha(T, t)]$$

or

$$\ln[d\alpha(t)/dt]_{T_a} + E^*/[RT_a] \text{ versus} - \ln [1 - \alpha_{T_a}(t)]$$

where  $T$  is temperature,  $t$  is time,  $\alpha(T, t)$  is the extent of conversion,  $d\alpha(T, t)/dT = y(T, t)$  or  $[d\alpha(t)/dt]_{T_a} = y(t)_{T_a}$  is the continuous heating or isothermal signal in a power-compensation DSC.  $E^*$  already has to be known.

(iii) The simplified fundamental differential equation for a quantitative DTA [15] is

$$\Delta H d\alpha(t)/dt + C_p dT/dt = \Delta T_{S-R}(t)/K(t) \\ + \Delta T_{S-E}(t)/K(t) \\ - \Delta T_{R-E}(t)/K(t) \\ + [\tau/K(t)]d[\Delta T(t)]/dt,$$

where  $\Delta H$  is the heat generated or absorbed by the sample,  $C_p$  is the heat capacity of the sample,  $K(t)$  is the thermal exchange coefficient being the calibration function of the measuring system,  $\Delta T_{S-R}$ ,  $\Delta T_{S-E}$  and  $\Delta T_{R-E}$  are the temperature gradients between the sample (S), reference (R) and environment (E),  $\tau$  is the time constant of the system. In the case of a sharp and massive reaction, the contribution of  $C_p$  term, the heat losses between the reference and its surrounding as well as the differential term might be neglected with relation to the huge contributions of the terms proportional to  $\Delta T_{S-R}$  and  $\Delta T_{S-E}$ . Thus the area of the DSC peak represents not only the heat of the reaction but also the heat losses between the sample and its surrounding, namely

$$\int \Delta T_{S-R}(t)/K(t)dt = \Delta H - \int \Delta T_{S-E}(t)/K(t)dt.$$

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